

## Factsheet:

# Solid oxide fuel cell (SOFC) using biogas

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DATE: 14/03/2023

VERSION: V4

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### Solid oxide fuel cell (SOFC) using biogas



#### Unique selling points:

- Energy production: electricity with heat as by-product
- High electrical conversion efficiency (60 %)
- Low environmental impact due to negligible emissions of SO<sub>2</sub>, CO, NO<sub>x</sub> and SO<sub>x</sub>

#### **Description of the technology**

The solid oxide fuel cell (SOFC; TRL: 9) uses chemical energy bound in gases such as hydrogen, carbon monoxide or upgraded biogas to produce electricity via electrochemical reactions, supplying also heat as by-product. Hence, it can be applied wherever biogas is produced, e.g. at municipal wastewater treatment plants (WWTP) with anaerobic sludge treatment, at industrial WWTPs with anaerobic pre-treatment or at agricultural or waste-based biogas plants. In the case biogas is used, methane (CH<sub>4</sub>) must be converted first into hydrogen (H<sub>2</sub>) and carbon monoxide (CO) in the reforming process. This can be done in two ways, internally using the SOFC and/or externally via a pre-reformer. More details regarding the reforming processes can be found in Saadabadi et al. 2019. After the reforming process, H<sub>2</sub> and CO are oxidized using oxygen ions in the SOFC in order to produce electricity.

Therefore, the SOFC consists of an anode, a cathode and an electrolyte and they are stacked layer-wise. At high temperatures, oxygen is reduced to oxygen ions at the cathode. The electrolyte transports the oxygen ions to the anode. At the anode, the fuel gases such as H<sub>2</sub> or CO are oxidized using the oxygen ion. The operating temperature is usually between 500-1200 °C, so that high temperature heat is available as a by-product. The technology is modular and has lower greenhouse gas emissions compared to traditional power generation, because harmful emissions such as SO<sub>2</sub>, CO, NO<sub>x</sub> and SO<sub>x</sub> are negligible from the electrochemical process of the SOFC operation (Al-Khori et al. 2021). Its electrical conversion efficiency is between 50% and 60% (Hussain and Yangping 2020, Saadabadi et al. 2019), which is higher than other electricity producing processes (e.g. combined heat and power plant) ranging between 30% and 40% (Saadabadi et al. 2019).

Using biogas as an alternative SOFC fuel to  $H_2$  or CO was proven to be viable (Saadabadi et al. 2019). However, raw biogas needs to be cleaned prior to the valorisation in a SOFC incl. the reforming process, since it usually contains traces of hydrogen sulphide ( $H_2S$ ), siloxanes, volatile organic compounds (VOC) and vapour condensates which can harm the SOFC.  $H_2S$  and siloxanes can cause erosion and degradation of the SOFC already at very low concentrations.

In Ultimate, a domestic-scale SOFC is used at the municipal WWTP valorising the cleaned biogas from the sludge treatment facility (CS Lleida). There, Aqualia uses the BlueGEN system,





developed by SOLIDpower SA (Solydera, since 03.10.22 (Solydera, 2022). BlueGEN is a commercial micro-CHP system targeted to small businesses, private households, and office buildings. Natural gas or biomethane can be used as the source of energy. With a gas input of 2.5 kW, the electrical power is up to 1.5 kW and the useable heat is 0.54 kW. Hence, it can yearly deliver electricity and heat of 13 MWh<sub>el</sub> and 7.4 MWh<sub>th</sub>, respectively (Bluegen 2023). The system is comprehensively described in Ferreira et al. 2019. To the author's knowledge, it will be the first SOFC operated with WWTP biogas at least in Spain.

#### Flow scheme of the technology

Fig. 1 shows the flow scheme of the SOFC demo plant in Lleida. The SOFC is marked with number 1. The other elements serve to clean the WWTP biogas before it is sent to the SOFC. Further details about the requirements and pre-treatment of the gas are provided in the section "Requirements of the technology and operating conditions".



Fig. 1 Solid oxide fuel cell demo plant in the frame of Ultimate

The SOFC (BlueGEN system) comprises a pre-reformer, the SOFC stack, an afterburner and several heat exchangers (Ferreira et al. 2019). In the pre-reformer, the  $CH_4$  reacts with the steam forming  $H_2$  and CO. Simultaneously the CO reacts with the steam and forms  $CO_2$  and  $H_2$ . The resulting gas is called syngas. The exhaust  $CH_4$  is then converted in the internal reformer in the SOFC stack. The endothermic methane steam reforming reaction rate leads to a significant local temperature drop near the anode inlet and hence to a temperature gradient inside the SOFC. This is unfavourable, because the key components of the SOFC are temperature-dependent (Cai et al. 2022).

The SOFC stack contains 70 planar anode-supported cells with an active area of 80 cm<sup>2</sup>. The cells are pressed and located between gas-diffusion layers and metallic interconnector plates. The anodes consist of standard nickel/yttrium-stabilized-zirconia (Ni-YSZ) cermet. A dense YSZ and a CGO (ceria-gadolinia) barrier layer serves as the electrolyte. The cathodes consist of





screen-printed (La, Sr)(Co, Fe)O<sub>3</sub>, which allow operating at temperatures between 650 °C and 850 °C.

The afterburner combusts the exhaust fuel ( $H_2$ , CO) and converts it into CO<sub>2</sub> and  $H_2O$ . The stream leaving the afterburner is reused to heat up the air and syngas streams.

#### **Pictures of the technology**



Fig. 2 Pictures of the side (left) and entrance (right) of the (bio) fuel cell pilot plant.

#### Synergetic effects and motivation for the implementation of the technology

#### ✓ SOFC: high electrical efficiency in energy production

As already outlined, the electrical conversion efficiency of a SOFC is quite high and ranges between 50% and 60% (Hussain and Yangping 2020, Saadabadi et al. 2019). Compared to other electricity producing processes (e.g. combined heat and power plant), the electrical conversion efficiency is higher, ranging between 50% and 60% compared to 30% and 40% (Saadabadi et al. 2019). The excess heat can be used for external heating systems. According to Ferreira et al. 2019, the SOFC has a combined efficiency of 82%, with 60% electrical and 22% heat efficiency.

#### ✓ Low environmental impact due to lower GHG emissions

The solid oxide fuel cell has lower greenhouse gas emissions to the atmosphere than a typical combustion process. Al-Khori et al. (2021) compared the CO<sub>2</sub>e release from the operation of a SOFC with natural gas to the CO<sub>2</sub>e emissions from a traditional power generation (the natural gas combined cycle), both located in Qatar, and showed a reduction of CO<sub>2</sub>e emissions of more than 80%. Hereby, it should be noted, that harmful emissions such as SO<sub>2</sub>, CO, NO<sub>x</sub> and SO<sub>x</sub> are negligible during the electrochemical process of the SOFC operation in contrast to a classical combustion process.

#### Requirements of the technology and operating conditions

In order to protect the SOFC from erosion and degradation, different requirements must be fulfilled. Biogas usually contains H<sub>2</sub>S, siloxanes, volatile organic compounds (VOC) and vapour condensates, which can harm the SOFC. Therefore, those substances must be removed. This can be done via a conventional filter for H<sub>2</sub>S, an activated carbon filter for siloxanes and VOC





and for removing the humidity via cooling to 5°C and filtering through a zeolite filter as shown by Giménez-Lorang et al. 2023 (Tab. 1). Here, it should be noted that the presented values for the gas components in Tab.1 are suggestions from Aqualia and not an official requirement from the SOFC supplier. Also for the humidity, there is no requirement from the supplier's side. However, in order to avoid condensation Aqualia suggests removing the condensate from the biogas prior to the SOFC via a condensate trap operated at a temperature below 5 °C.

Parameter	Units	Min	Max	Reference
H <sub>2</sub> S	mg/Nm <sup>3</sup>	<20		
Siloxanes	mg Si/Nm <sup>3</sup>	<0,05= LOQ		Giménez-Lorang et al. 2023
VOC	mg/Nm <sup>3</sup>	<0,02= LOQ		
Pressure	mbar	15	25	SOLIDpower 2019
Temperature (dew point) for condensate trap	°C	<5		Giménez-Lorang et al. 2023
Temperature in the SOFC	°C	ca. 750		SOLIDpower 2019

#### Tab. 1 Typical ranges for crucial parameters (LOQ – limit of quantification)

Furthermore, the SOFC should be operated continuously due to the very high operating temperatures (Tab. 1). Compared to a CHP, which can be operated at various levels with reasonable efficiency, this is a disadvantage. The continuous operation of the SOFC can be maintained via an uninterruptible power supply and a biogas buffer in the case of undesired interruptions in biogas production. Due to the operation of the SOFC with biogas containing methane, extra attention should be paid to the rules for operating technologies in an explosive atmosphere.

#### **Key performance indicators**

The electrical conversion efficiency of a SOFC is quite high and ranges between 50% and 60% (Tab. 2). Hereby, the performance of a SOFC highly depends on the purity of the fuel gas. When using conventional nickel-based anodes,  $H_2S$  poisons the anode by converting Ni into Ni-sulfides (Saadabadi et al. 2019). Those attach on the anode and reduce its performance.

Parameter	Unit	min-max	References
Electrical conversion efficiency	%	50 – 60	Hussain and Yangping 2020, Saadabadi et al. 2019; Ferreira et al. 2019
Energy recovery potential for usable heat	%	22-25	Ferreira et al. 2019, Bosch 2023
Power density	mW/cm²	245-1400	Saadabadi et al. 2019, Hussain and Yangping 2020,

Tab. 2 Key performance indicators for biogas fuelled SOFCs

Either  $H_2S$  is removed upstream to the SOFC or anodes with a high resistance against  $H_2S$  are used. In the latter case, the advantage is that the removal of  $H_2S$  from the biogas as an additional treatment step would not be necessary anymore. Sulfur tolerant anodes are based



on nickel-free electrodes such as perovskites. Saadabadi et al. 2019 and Hussain and Yangping 2020 provide a detailed overview on the recent developments of sulfur tolerant anodes. Aguilar et al. (2004) tested for example a strontium doped lanthanum vanadate anode, which could be successfully operated with H<sub>2</sub>S contents below 5%.

The achievable power density depends on the electrode materials, the type of electrolyte and the operating temperature. 1200 mW/cm<sup>2</sup> were for example achieved with a SCO/CFSCO anode and LSGM as electrolyte at a temperature of 800 °C (Zhu and Lu, 2008).

#### Links to related topics and similar reference projects

Process/technologies	Reference		
Anaerobic membrane reactor	Case study "Spernal" (NextGen)		
(AnMBR)			
Anaerobic high rate reactor (AAT)	Case study "Shafdan" & Case study "Karmiel"		
	(Ultimate)		
Anaerobic digestion	Factsheet in TEB		

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